## IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Currently Amended): A process for the preparation of an aqueous polymer dispersion by free radical aqueous emulsion polymerization of comprising polymerizing at least one ethylenically unsaturated compound (monomer) in the presence of at least one dispersant, wherein

- a) in into a reaction vessel at a temperature which is less than or equal to the starting reaction temperature  $T_S$ ,
- a<sub>1</sub>) at least one portion of demineralized water,
- a<sub>2</sub>) at least one portion of at least one oil-soluble free radical initiator,
- a<sub>3</sub>) at least one portion of at least one dispersant,
- a<sub>4</sub>) if appropriate optionally, a portion of the at least one monomer and
- a<sub>5</sub>) if appropriate optionally, a portion of at least one water-soluble free radical initiator are initially taken added to form a reaction mixture in the reaction vessel, thereafter
- b) the reaction mixture obtained is, if appropriate optionally, heated to the starting reaction temperature T<sub>S</sub>, and thereafter
- c) the following are metered into the reaction mixture:
- c<sub>1</sub>) if appropriate optionally, the remaining amount of demineralized water,
- c<sub>2</sub>) if appropriate optionally, the remaining amount of the at least one oil-soluble free radical initiator,
- c<sub>3</sub>) if appropriate optionally, the remaining amount of the at least one dispersant,
- c<sub>4</sub>) the total amount or, if appropriate optionally, the remaining amount of the at least one monomer and
- c<sub>5</sub>) the main amount of the at least one water-soluble free radical initiator, and

d) the reaction mixture is heated to an end reaction temperature T<sub>E</sub> during the metering of the at least one monomer, and wherein

the at least one water-soluble free radical initiator has initiators being understood as meaning those which have a solubility of ≥ 1% by weight at 20°C and atmospheric pressure in demineralized water, while and the at least one oil-soluble free radical initiators being understood as meaning those which have initiator has a solubility of < 1% by weight under the abovementioned conditions and the total amount of water being such that the aqueous polymer dispersion obtained has a solids content of from 20 to 70% by weight.

Claim 2 (Original): The process according to claim 1, wherein the at least one water-soluble free radical initiator initiates a free radical polymerization reaction of the at least one monomer at the starting reaction temperature T<sub>S</sub>.

Claim 3 (Currently Amended): The process according to either of claims 1 and 2 Claim 1, wherein the at least one oil-soluble free radical initiator has a half-life of  $\geq$  10 hours at the starting reaction temperature  $T_S$  and a half-life of  $\leq$  5 hours at the end reaction temperature  $T_E$ .

Claim 4 (Currently Amended): The process according to any of claims 1 to 3 Claim 1, wherein  $T_E \ge T_S + 10^{\circ}$ C.

Claim 5 (Currently Amended): The process according to any of claims 1 to 4 Claim 1, wherein  $T_S$  is from  $\geq$  30 to  $\leq$  120°C and  $T_E$  is from  $\geq$  80 to  $\leq$  200°C.

Claim 6 (Currently Amended): The process according to any of claims 1 to 5 Claim 1, wherein the amount of water-soluble and oil-soluble free radical initiator is in each case from 0.01 to 5% by weight, based on the total amount of monomer.

Claim 7 (Currently Amended): The process according to any of claims 1 to 6 Claim 1, wherein the pressure during the polymerization is chosen so that the reaction mixture does not boil at any time.

Claim 8 (Currently Amended): The process according to any of claims 1 to 7 Claim 1, wherein the at least one water-soluble free radical initiator used is a mono- or di-alkali metal or ammonium salt of peroxodisulfuric acid.

Claim 9 (Currently Amended): The process according to any of claims 1 to 8 Claim 1, wherein the at least one oil-soluble free radical initiator used is [[a]] at least one compound selected from the group consisting of tert-butyl peroxy-2-ethylhexanoate (Trigonox® 21), tert-amyl peroxy-2-ethylhexanoate, tert-butyl peroxybenzoate (Trigonox® C), tert-amyl peroxybenzoate, tert-butyl peroxyacetate, tert-butyl peroxy-3,5,5-trimethylhexanoate (Trigonox® 42 S), tert-butyl peroxyisobutanoate, tert-butyl peroxydiethylacetate, tert-butyl peroxypivalate, tert-butyl peroxyisopropylcarbonate, (Trigonox® BPIC) and tert-butyl peroxy-2-ethylhexylcarbonate (Trigonox® 117).

Claim 10 (Currently Amended): The process according to any of claims 1 to 9 Claim 1, wherein the reaction mixture is kept at the end reaction temperature T<sub>E</sub> for at least a further 30 minutes after the end of the monomer metering.

Claim 11 (Currently Amended): The process according to any of claims 1 to 10 Claim 1, wherein the reaction mixture is stripped with inert gas and/or steam after the end of the monomer metering.